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24 **Gaseous emissions from the storage of untreated slurries and the**  
25 **fractions obtained after mechanical separation**

26

27 E. Dinuccio<sup>a,\*</sup>, W. Berg<sup>b</sup>, P. Balsari<sup>a</sup>

28

29 <sup>a</sup> Department of Agriculture, Forestry, Environmental Engineering and Land Based Economics  
30 (DEIAFA) Mechanics Section - Turin University via Leonardo da Vinci 44, 10095 Grugliasco (TO)  
31 Italy.

32 <sup>b</sup> Institute of Agricultural Engineering Bornim (ATB), Max-Eyth-Allee 100, D-14469 Potsdam,  
33 Germany.

34 \*Corresponding author. Tel. +39 0116708844; Fax: +39 0116708591; E-mail address:

35 [elio.dinuccio@unito.it](mailto:elio.dinuccio@unito.it)

36

37 **Abstract**

38 A laboratory scale study was set up to investigate the ammonia (NH<sub>3</sub>), nitrous oxide (N<sub>2</sub>O), carbon  
39 dioxide (CO<sub>2</sub>) and methane (CH<sub>4</sub>) emissions during storage of untreated pig and cattle slurry and  
40 the fractions (solid and liquid) obtained by mechanical separation. The solid and liquid fractions  
41 were obtained from the same untreated slurry by means of a lab scale mechanical separator.

42 The manures were stored for a period of 30 days in open vessels (1500 cm<sup>3</sup> capacity) in two  
43 temperature controlled rooms which were kept at 5±0.5 °C and 25±0.2 °C. Gaseous emissions were  
44 determined using a dynamic chamber method and Infrared Photoacoustic Detection (IPD).

45 Over the storage period, gaseous emissions from pig manures were significantly (P<0.05) higher  
46 than those from cattle manures. N<sub>2</sub>O fluxes of up to 232 mg m<sup>-2</sup> h<sup>-1</sup> were measured but from pig  
47 solid fraction only. Between 40.8% (from pig liquid fraction stored at 25 °C) and 3.60% (from  
48 untreated cattle slurry stored at 25 °C) of the initial nitrogen content of the manures was lost as

49 NH<sub>3</sub>. Over the 30-days storage period, the predominant emission of carbon was in the CO<sub>2</sub> form.  
50 Total C-CH<sub>4</sub> losses expressed as a percent of the carbon initially present in the volatile solids (C-  
51 VS) ranged from 0.60% to 12.8% for pig manures and from 0.23% to 1.56% for cattle manures. The  
52 mechanical separation of cattle slurry increased by up to 30% the emissions of CO<sub>2</sub> equivalents to  
53 the atmosphere during the storage of the separated fractions if compared with the slurries. Results  
54 indicated that NH<sub>3</sub>, N<sub>2</sub>O, CO<sub>2</sub> and CH<sub>4</sub> emissions were affected by the interaction between a  
55 number of variables, including storage temperature, chemical characteristics and type of manure.  
56 Results also indicated that mechanical separation does not reduce emissions but has the potential to  
57 increase the emissions of CO<sub>2</sub> equivalents to the atmosphere during the storage of the separated  
58 fractions.

59

60 Keywords: ammonia, greenhouse gas emissions, manure storage, slurry separation.

61

62

63

## 1. Introduction

64 Animal excreta can contribute to eutrophication of groundwater and surface waters as a result of  
65 nitrogen (N) and phosphorous (P) enrichment (EEA, 2005) and are considered an important source  
66 of ammonia (NH<sub>3</sub>), nitrous oxide (N<sub>2</sub>O), carbon dioxide (CO<sub>2</sub>) and methane (CH<sub>4</sub>) production (Van  
67 Der Hoek, 1998; Amon et al., 2001). While N<sub>2</sub>O, CO<sub>2</sub>, and CH<sub>4</sub> are greenhouse gases affecting the  
68 global environment and climate change, NH<sub>3</sub> contributes to eutrophication and acidification of soils  
69 and also indirectly contributes to N<sub>2</sub>O emissions by increasing the N-cycling in natural ecosystems  
70 (Olesen, 2005). Modern intensive animal production methods have increased the volume of manure  
71 in the slurry form (Menzi et al., 2002). Several techniques have been developed to manage livestock  
72 slurries as cheaply and conveniently as possible and to reduce potential risks of environmental  
73 pollution. Among these techniques, solid-liquid separation is a technology that separates slurry into  
74 a larger liquid fraction and a minor solid fraction which has a greater concentration of nutrients than

75 the liquid (Kroodsma, 1986; Møller et al., 2000). This could enable more cost-effective transfer of  
76 nutrients from areas of high livestock density where they may be in surplus to areas with a lower  
77 livestock density. Nevertheless, little data concerning  $\text{NH}_3$ ,  $\text{N}_2\text{O}$ ,  $\text{CH}_4$  and  $\text{CO}_2$  emissions during  
78 storage of both liquid and solid fractions are currently available.

79 In consequence a laboratory-scale trial was carried out to better characterize the main parameters  
80 affecting  $\text{NH}_3$  and GHG emissions from the storage of untreated liquid manure and both the solid  
81 and liquid fractions derived from mechanical separation of slurry. The following aspects have been  
82 analyzed:

83 1) the  $\text{NH}_3$ ,  $\text{CO}_2$ ,  $\text{CH}_4$  and  $\text{N}_2\text{O}$  emissions from the storage of:

84 A. cattle and pig untreated liquid manure

85 B. solid fractions obtained from both untreated liquid manure after solid-liquid  
86 separation

87 C. liquid fractions obtained from both untreated liquid manure after solid-liquid  
88 separation

89 2) the effects of temperature and chemical characteristics of the three products listed in point 1)  
90 on such emissions.

91

## 92 **2. Materials and methods**

93 The trials were carried out at Leibniz-Institute for Agricultural Engineering Potsdam-Bornim  
94 (ATB), Germany, in environmentally controlled conditions by means of two climatic rooms.

95 Fresh slurry was collected from commercial farms. The next day (cattle; pig two days after) it was  
96 separated and stored in vessels in the emission lab of the institute and measurements began.

97 The solid and liquid fractions (B and C) were obtained from the same pig and cattle untreated slurry  
98 (A) by means of a laboratory-scale mechanical separator. This latter was made up of (Fig. 1): a  
99  $1500\text{ cm}^3$  bowl with handle; a stainless steel disc (screen) with circular holes 2.3 mm in diameter; a  
100 stainless steel blade integral with a crank; a container collecting the liquid fraction.

101 A press zone was created fitting the blade to the disc by means of a horizontal bar and a spring.  
 102 After filling the bowl with the untreated slurry, the blade is manually rotated using the crank and  
 103 the slurry separated in the press zone. The liquid fraction runs through the disc's holes into the  
 104 container while the solid fraction remains in the bowl and is collected afterwards. The total input of  
 105 each untreated slurry (100 kg), as well as the amounts of solid (18.1 kg for cattle and 7.80 kg for  
 106 pig) and liquid (81.9 kg for cattle and 92.2 kg for pig) recovered, were weighed and recorded. The  
 107 bulk density of the solid fractions (cattle and pig) was estimated to be  $0.40 \text{ t m}^{-3}$ .  
 108 Immediately after mechanical separation, samples of  $1000 \text{ cm}^3$  of each of the investigated materials  
 109 were stored for a period of 30 days in open vessels ( $1500 \text{ cm}^3$  capacity, 0.20 m height, 0.10 m base  
 110 diameter and 0.095 m top diameter) in two temperature-controlled rooms which were kept at  $5 \pm 0.5$   
 111 and  $25 \pm 0.2 \text{ }^\circ\text{C}$ . During the test period observations of crust formation and reduction of volume were  
 112 carried out. Four replicates of each product were tested so that for each type of untreated liquid  
 113 manure (pig or cattle) a total of 12 vessels were used per climate room.  
 114 The samples were analysed for pH, total solids (TS), volatile solids (VS), total Kjeldhal nitrogen  
 115 (TKN), total ammoniacal nitrogen (TAN), and organic acids at the beginning and at the end of the  
 116 investigation period. Initial and final slurry analyses are given in Table 1.  
 117  
 118 Flux measurements were carried out using infrared photoacoustic detection (IPD) and the dynamic  
 119 chamber method described by Berg et al. (2006). This method allows the comparison of the effect  
 120 of different treatments on gaseous emissions during manure storage, under standardized  
 121 experimental conditions. Different conditions, such as volume to surface ratio of the manure stores,  
 122 in the lab and on farms may yield different gas fluxes. Therefore, this fluxes cannot be used for  
 123 calculating fluxes from on farm storage facilities without further validation. Accordingly, the  
 124 slurries were stored in open vessels using the dynamic chamber method set up only during  
 125 measurements. Before starting the measurements each vessel was closed with an air-tight lid  
 126 provided with two ports for air inlet and outlet (Fig. 2). Air inlet port was connected in an airtight

127 way with a flow meter and a compressor. The headspace (chamber) between the slurry surface and  
128 the lid was then ventilated with compressed air to create an airflow through the dynamic chamber.  
129 The air exchange inside the chambers was adjusted by the flow meters so that the air in the  
130 headspace was always changed once per minute. Measurements were carried out four times a week  
131 according to the following scheme:

- 132 1) lid closure at time  $t = 0$  min;
- 133 2) between  $t=0$  and  $t= 20$  min the chamber was only ventilated to achieve steady conditions inside  
134 the chamber;
- 135 3)  $t= 20$  min beginning of the exhaust air sampling;
- 136 4)  $t= 36$  min end of the exhaust air sampling and vessel opening.

137 The gas concentrations in the inlet (atmospheric) and outlet (exhaust) air were analyzed by the  
138 INNOVA system 1312 Photoacoustic Multi-gas Monitor and Multipoint Sampler. The system  
139 provided a real time analysis of 4 gases ( $\text{NH}_3$ ,  $\text{N}_2\text{O}$ ,  $\text{CH}_4$  and  $\text{CO}_2$ ) plus water vapour. Measured  
140 data were related to standard conditions ( $25^\circ\text{C}$  and  $100\text{ kPa}$ ) and stored in a database. Exhaust air  
141 leaving each chamber was sampled for 16 min. The instrument needed 2 min to analyze one sample,  
142 thus, 8 values were recorded on each measurement occasion. The first 3 values were discarded and  
143 the mean of the remaining 5 recorded values was considered representative for the measurement.  
144 Gas fluxes  $F_j$  in  $\text{mg m}^{-2} \text{ h}^{-1}$  were determined according to:

$$145 \quad F_j = Q \frac{(C_{ex,j} - C_{in,j})}{A} \quad (1)$$

146 where  $C_{in,j}$  is the  $\text{NH}_3$ ,  $\text{N}_2\text{O}$ ,  $\text{CH}_4$  or  $\text{CO}_2$  concentration of air inlet the chamber in  $\text{mg m}^{-3}$ ;  $C_{ex,j}$  is  
147 the  $\text{NH}_3$ ,  $\text{N}_2\text{O}$ ,  $\text{CH}_4$  or  $\text{CO}_2$  concentration of air outlet the chamber in  $\text{mg m}^{-3}$ ;  $Q$  is the air flow rate  
148 through the chamber in  $\text{m}^3 \text{ h}^{-1}$ ;  $A$  is the area of emitting surface covered by the chamber in  $\text{m}^2$ .  
149 Time evolution of the gas fluxes were approximated by spline approximation functions, and by  
150 integration of such approximations using adaptive Simpson quadrature formulas (Bronshtein et al.,

2003) cumulative losses  $\varphi_j$  in mg vessel<sup>-1</sup> of each gas over the storage period (30 days) were estimated.

Since measurements were carried out with 1000 cm<sup>3</sup> of all substrates respectively, in order to assess the effect of mechanical separation on gaseous emissions, cumulative losses were corrected as follows:

$$\Phi_j = \varphi_j \cdot \rho \quad (2)$$

where  $\Phi_j$  is the corrected cumulative loss of a specified gas in mg vessel<sup>-1</sup>;  $\rho$  is a correction factor that takes into account the mass  $Sc$  (kg) of separated liquid and solid fractions obtained after separation of the untreated slurry  $Mc$  (kg), and the amount  $Me$  (kg) of untreated slurry, liquid and solid fractions used for emission trials:

$$\rho = \frac{Sc}{Mc} \cdot \frac{1}{Me} \quad (3).$$

The  $\rho$  values used are summarized in Table 1.

During storage trials, volume and surface area in contact with the air were the same for all tested materials. Nevertheless, in practical conditions slurries are stored within tanks and solid fraction in heaps on platforms. The slurry NH<sub>3</sub> emitting area is the horizontal cross section of the storage tank, while for solid material it may be considered the surface area of a hypothetical frustum of cone representing the shape of the heap. Considering an angle of repose of 1<sup>1</sup>/<sub>2</sub> : 1 (horizontal : vertical) (CNMP, 2002), the surface/volume ratio for the pig solid fraction was calculated to be 1.83 times as much as pig slurry and 2.44 times as much as cattle untreated slurry for the cattle solid fraction. Thus, to be able to assess the effect of mechanical separation on NH<sub>3</sub> emissions, measured NH<sub>3</sub> emissions from pig solid fraction and cattle solid fraction were therefore multiplied by 1.83 and by 2.44 respectively, assuming that the emissions per unit area were homogeneous. The emitting surface area of the liquid fraction was assumed to be that of the untreated slurry.



174 To consider the effect of slurry mechanical separation on GHG emissions as a whole, the  $IC_jI$  were  
175 converted into CO<sub>2</sub> equivalents by the Global Warming Potential (GWP) of the gases (NH<sub>3</sub>: 3.1,  
176 N<sub>2</sub>O: 310, CH<sub>4</sub>: 21) (IPCC, 1997).

177

178 Significant differences in results and all possible interactions were investigated using the ANOVA  
179 procedure. Before analysis some of the parameters were log-transformed in order to fit a normal  
180 distribution. For all the statistics, a significant level of  $P = 0.05$  was applied. Assumption of equal  
181 variance of different groups was tested using Bartlett's test. All statistical analyses were performed  
182 with SPSS 12.0 for Windows.

183

### 184 **3. Results**

#### 185 **3.1 Slurry properties**

186 After mechanical separation the liquid fractions produced by mechanical separation showed  
187 significant reductions of TS and VS (Table 1). In contrast, the pH, TAN and TKN concentrations of  
188 the liquid fractions were very similar to those of the untreated slurries. As expected, the TS and VS  
189 content of the solid fractions were significantly greater than those for the untreated slurries. The  
190 TKN content of the pig solid fraction was almost double the TKN content of the pig untreated  
191 slurry, while the TKN content of the cattle solid fraction was approximately 1.4 times lower than  
192 the TKN content of the cattle untreated slurry.

193 Analysis of the manures at the end of each experiment are given in Table 2 together with volume  
194 reductions over the storage period.

195 Water evaporation occurred in all the samples throughout the storage period. As expected,  
196 evaporation was higher from materials stored at 25 °C than 5 °C and was responsible for volume  
197 reductions up to 45% of the stored slurries and of the relative increase of TS and VS amounts.

198 Appreciable volume reduction (30.6%) occurred for cattle solid fraction stored at 25 °C, low

199 reductions were observed for solid materials stored at 5 °C while no volume reduction occurred for  
200 pig solid fraction stored at 25 °C.

201

## 202 3.2 Gaseous emissions

### 203 3.2.1 N<sub>2</sub>O emissions

204 Over the storage period (30 days), no N<sub>2</sub>O fluxes were measured from any material stored at 5 °C.  
205 N<sub>2</sub>O emissions from cattle and pig slurries stored at 25 °C occurred on a very few occasions only,  
206 e.g. when the crust dried up, but the overall amounts were negligible. Very low concentrations,  
207 sometimes slightly above the background concentration of N<sub>2</sub>O, were also measured from the cattle  
208 solid fraction. Appreciable N<sub>2</sub>O fluxes were measured only from the pig solid fraction stored at  
209 25 °C (Fig. 3). N<sub>2</sub>O emissions started 8 days after the beginning of the storage period and reached a  
210 peak of 232 mg m<sup>-2</sup> h<sup>-1</sup> at day 21. After that peak, the N<sub>2</sub>O flux rapidly decreased to reach values  
211 close to zero at day 25. The total nitrogen loss via the N<sub>2</sub>O pathway accounted for the 4.71% of the  
212 initial total Kjeldahl nitrogen (TKN) content of the solid manure (Table 3).

213

### 214 3.2.2 NH<sub>3</sub> emissions

215 Total losses of NH<sub>3</sub>-N, expressed as a percentage of the initial TKN, (Table 3) ranged from 3.60%  
216 (from untreated cattle slurry stored at 25 °C) to 40.8% (from pig liquid fraction stored at 25 °C).  
217 Under the same storage conditions, there were no significant (P>0.05) differences between NH<sub>3</sub>  
218 fluxes from untreated pig slurry and from its liquid fraction (Fig. 4). In contrast, NH<sub>3</sub> fluxes from  
219 untreated cattle slurry were significantly less than from its liquid fraction. NH<sub>3</sub> emissions were  
220 higher at 25 °C than at 5 °C storage conditions, except when considering the pig solid fraction.  
221 From this, significantly (P<0.05) higher NH<sub>3</sub> fluxes at 25 °C than at 5 °C were measured only at the  
222 beginning of the storage period, while, after day 8 NH<sub>3</sub> fluxes were significantly lower at 25 °C  
223 than at 5 °C storage conditions.

224

### 225 3.2.3 CO<sub>2</sub> and CH<sub>4</sub> emissions

226 During pig and cattle manure storage, the predominant emission of carbon was as CO<sub>2</sub> (Fig. 5 and  
227 Table 3). Total losses of C-CO<sub>2</sub> expressed as a percentage of the carbon initially present in the  
228 volatile solids (C-VS) of the manures ranged from 7.76% (from cattle untreated slurry stored at  
229 5 °C) to 33.4% (from pig liquid fraction stored at 25 °C). CO<sub>2</sub> losses were always higher at 25 °C  
230 and lower at 5 °C storage conditions.

231 Under the same storage conditions, CH<sub>4</sub> fluxes from the untreated slurries and from their liquid  
232 fractions were not different ( $P>0.05$ ) (Fig. 6), but total C-CH<sub>4</sub> losses over the storage period,  
233 expressed as a fraction of initial C-VS content, were significantly ( $P<0.05$ ) higher from liquid  
234 fractions than from untreated slurries (Table 3). Under all storage conditions, total C-CH<sub>4</sub> losses  
235 were higher from pig than from cattle slurries. C-CH<sub>4</sub> losses ranged from 0.60% to 12.8% for pig  
236 manures and from 0.23% to 2.19% of the initial C-VS content for cattle manures. C-CH<sub>4</sub> losses  
237 from pig manures were always consistently higher at 25 °C than those at 5 °C. However, the  
238 emissions of CH<sub>4</sub> were only observed to be significantly ( $P<0.05$ ) higher from cattle slurries stored  
239 at 25 °C than at 5 °C during the first 3 days of storage. Thereafter, the emissions were lower from  
240 cattle slurries stored at 25 °C than at 5 °C. C-CH<sub>4</sub> losses from cattle and pig solid fractions were  
241 always significantly lower at 25 °C than at 5 °C storage.

242

### 243 3.2.4 Effect of slurry solid-liquid separation on gaseous emissions

244 Figure 7 shows the NH<sub>3</sub>, CO<sub>2</sub> and CH<sub>4</sub> losses based on the corrected cumulative losses  $IC_jI$  and  
245 expressed as a percentage of the  $IC_jI$  calculated for the untreated slurries (pig and cattle). It can be  
246 seen that for pig slurry the combined emissions measured from the storage of the liquid and solid  
247 fractions resulted in reduced NH<sub>3</sub> losses compared to the storage of the untreated pig slurry.  
248 However for cattle slurry, the combined NH<sub>3</sub> losses measured from the storage of the liquid and  
249 solid fractions were 7% and 45% higher than those measured from the untreated cattle slurry stored  
250 at 25 °C and 5 °C respectively.

251 The emissions from the storage of the two fractions increased the CO<sub>2</sub> emissions from 8% (when  
252 compared to untreated pig slurry stored at 5 °C) to 104% (when compared to untreated cattle slurry  
253 stored at 25 °C). During the storage of both liquid and solid fractions, CH<sub>4</sub> losses were 3% higher  
254 for pig untreated slurry stored at 25 °C and 4% higher for cattle untreated slurry stored at 5 °C.  
255 Instead, solid-liquid separation reduced CH<sub>4</sub> emissions by 8% for pig untreated slurry stored at 5 °C  
256 and by 9% for cattle untreated slurry stored at 25 °C.  
257 Combining the emissions of CO<sub>2</sub> equivalents from both liquid and solid fractions (Fig. 8), they  
258 resulted in increased greenhouse gases emissions compared to the storage of the untreated slurries,  
259 except when considering the pig untreated slurry stored at 5 °C. In this latter case the mechanical  
260 separation had no effect in combined emissions of CO<sub>2</sub> equivalents.

261

#### 262 **4. Discussion**

263 The small N<sub>2</sub>O fluxes from cattle and pig slurries storage can be explained by the absence of crust  
264 during most of the storage period. N<sub>2</sub>O may be emitted during storage of manure either as a by-  
265 product of incomplete ammonium oxidation or as a by-product of incomplete denitrification  
266 (Oenema et al., 2001). The condition in liquid manure is strictly anaerobic, and neither process  
267 occurs. In contrast, authors (e.g. Sommer et al., 2000; Berg et al., 2006) found N<sub>2</sub>O production from  
268 stored slurries, but only when a dry crust formed on the surface. These emissions occurred since  
269 surface crust may contain a mosaic of anaerobic and aerobic micro-sites which are favourable for  
270 N<sub>2</sub>O production. Dry conditions, together with air filled porosity, may explain the occurrence of  
271 N<sub>2</sub>O production from pig solid fraction samples. On the other hand, separation of cattle slurry  
272 produced a fibrous solid fraction with a compacted structure, this might have created an  
273 environment with an oxygen concentration unsuitable for N<sub>2</sub>O production.  
274 Results confirm a positive relationship between ammonia emission and temperature found by other  
275 studies (e.g. Ni, 1999; Dewes, 1996), but not in the case of the pig solid fraction. Total losses from  
276 the pig solid fraction were 7.12 and 5.57% of the initial TKN content at 5 and at 25 °C storage

277 conditions respectively. This may be explained by ammonium oxidation by nitrifying micro-  
 278 organisms with  $\text{N}_2\text{O}$  production.  $\text{NH}_3$  emission from manure decreased, therefore, as a greater  
 279 proportion of the  $\text{NH}_4\text{-N}$  was oxidized by nitrifying micro-organisms.

280  $\text{CH}_4$  losses from pig slurries significantly increased with temperature (Table 3). This is confirmed  
 281 by results of other studies (e.g. Husted, 1994), in which an increase of the  $\text{CH}_4$  production with air  
 282 storage temperature was also found. The lowest  $\text{CH}_4$  emissions from cattle slurries stored at 25 °C  
 283 with respect to those obtained at 5 °C were probably caused by the high water losses from the  
 284 slurries over time. As a consequence, a relative increase in concentration of constituents, such as  
 285  $\text{NH}_3$  and organic acids, which could be inhibitory to the methanogens (Kalle and Menon, 1984;  
 286 Angelidaki et al., 1999), occurred. This was proved by the  $\text{CH}_4$  fluxes from both untreated cattle  
 287 slurry and liquid fraction stored at 25 °C which were observed to be high at the beginning of the  
 288 storage and to gradually decrease over time (Fig. 6). Additionally, Table 2 shows for cattle slurries  
 289 a relative increase in concentration of organic acids, which can be inhibitory to the methanogens, at  
 290 the end of the storage compared to the beginning of the storage (Table 1). The combined effect of  
 291 temperature and slurry concentration had no effect on  $\text{CH}_4$  losses from pig slurries, probably due to  
 292 a more active methanogens population. According to Massé et al. (2003), manure from different  
 293 animals probably contains different species of anaerobic bacteria, which may be better adapted or  
 294 acclimatized to inhibitive components such as organic acids.

295  $\text{CH}_4$  emission reductions from the cattle and pig solid fractions stored at 25 °C could also be  
 296 explained by the high water losses over time. From the beginning of the storage period, when solid  
 297 fractions started to dry, air entered the pores previously filled with water. The high water losses  
 298 combined with low volume ( $1000\text{ cm}^3$ ) of the samples in storage, resulted in a substantial reduction  
 299 of the anaerobic zone inside the cattle and pig solid fractions stored at 25 °C. Methanogenesis is  
 300 inhibited by low moisture content and oxygen availability in the manure. Furthermore, most studies  
 301 show  $\text{CH}_4$  emission reductions due to the methane oxidation during the passage through the porous  
 302 surface layers of manure heaps (Olesen, 2005). Biological  $\text{CH}_4$  oxidation is a process whereby

methane is oxidised to carbon dioxide and water by methane oxidizing bacteria (methanotrophs) under aerobic conditions (Cicerone and Oremland, 1988; Kotsyurbenco, 2005). The substantial reduction of the anaerobic zone over time and the biological CH<sub>4</sub> oxidation in the outer layers could be the causes for lower CH<sub>4</sub> emissions from pig and cattle solid fractions stored at 25 °C.

307

## 308 **5. Conclusion**

Results from this study show that emissions of NH<sub>3</sub> and GHGs during the storage of animal manures are influenced by different factors. Since emissions of NO<sub>2</sub>, NH<sub>3</sub>, CO<sub>2</sub> and CH<sub>4</sub> are affected by microbiological, chemical, and physical processes, complex interactions exist. This requires a whole system approach when pollutant abatement technologies have to be adopted. Evidence from the present study suggests that mechanical separation of cattle and pig slurries does not reduce emissions but has the potential to increase the emissions of CO<sub>2</sub> equivalents to the atmosphere during the storage of the separated fractions by up to 30% if compared with the untreated slurries. The emission potential of pig slurry was up to 3 times higher than that of cattle slurry. It was determined under the laboratory conditions and assumptions as described. Thus, to confirm these results, experiments should be made under on-farm storage conditions.

319

## 320 **Acknowledgements**

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325

326

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382 **Figure legends**

383 Fig. 1. Main components of the lab-scale mechanical slurry separator.

384 Fig. 2. Schematic diagram of the sampling system.

385 Fig. 3. Nitrous oxide (N<sub>2</sub>O) fluxes from pig solid fraction stored at 25 °C. Error bars indicate standard error (number of  
386 observations = 4).

387 Fig. 4. Emission fluxes of ammonia (NH<sub>3</sub>) during storage of the tested materials at 5 °C and 25 °C. Error bars indicate  
388 standard error (number of observations = 4).

389 Fig. 5. Emission fluxes of carbon dioxide (CO<sub>2</sub>) during storage of the tested materials at 5 °C and 25 °C. Error bars  
390 indicate standard error (number of observations = 4).

391 Fig. 6. Emission fluxes of methane (CH<sub>4</sub>) during storage of the tested materials at 5 °C and 25 °C. Error bars indicate  
392 standard error (number of observations = 4).

393 Fig. 7. Corrected cumulative loss  $\Phi_j$  of NH<sub>3</sub>, CO<sub>2</sub> and CH<sub>4</sub> of the investigated samples in relation to the  $\Phi_j$  from  
394 untreated slurries (pig and cattle) samples.

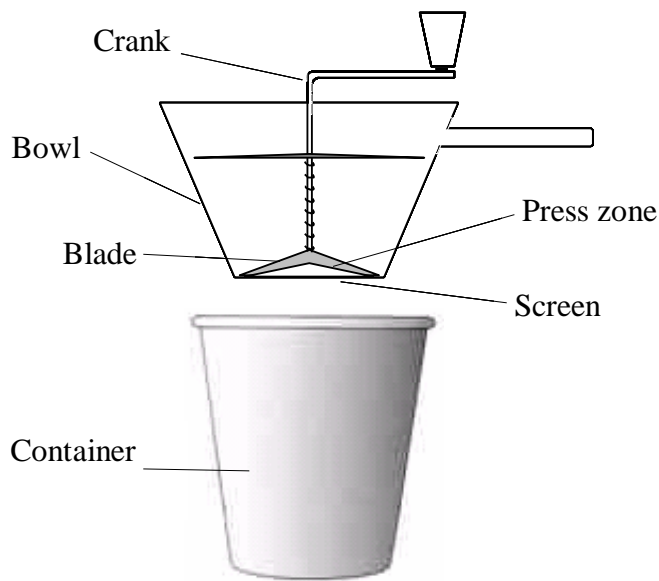
395 Fig. 8. Climatic warm potential of untreated slurry (pig and cattle), liquid and solid fractions expressed as CO<sub>2</sub>  
396 equivalents calculated from the cumulated emissions of the single trace gases.

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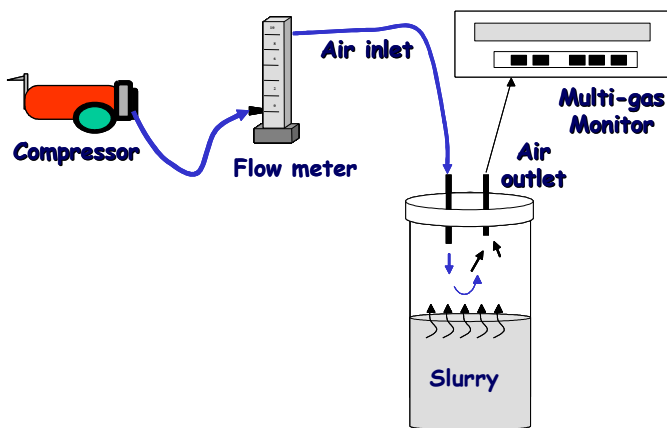
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402 Fig. 1.

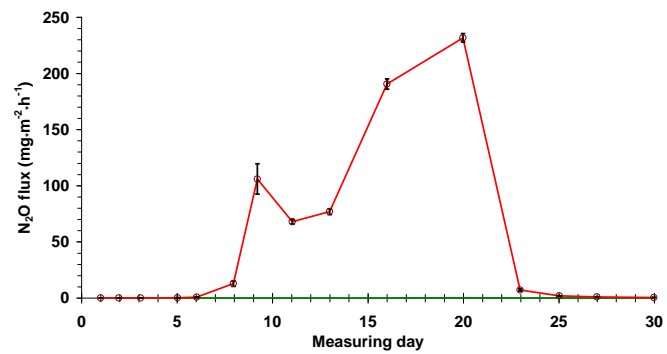
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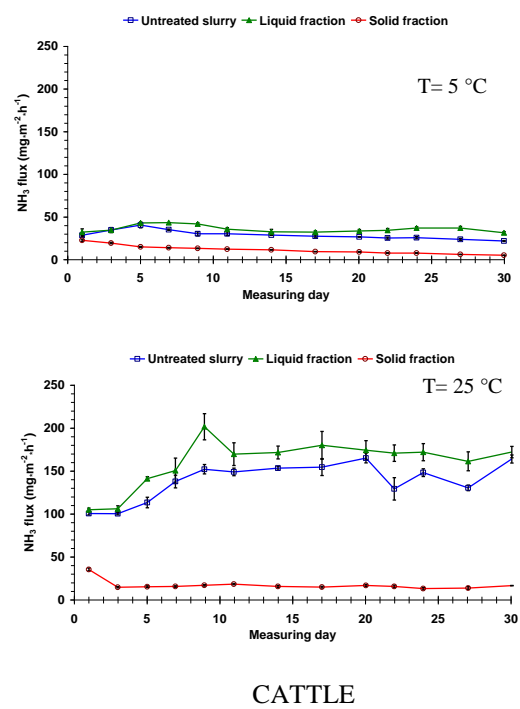
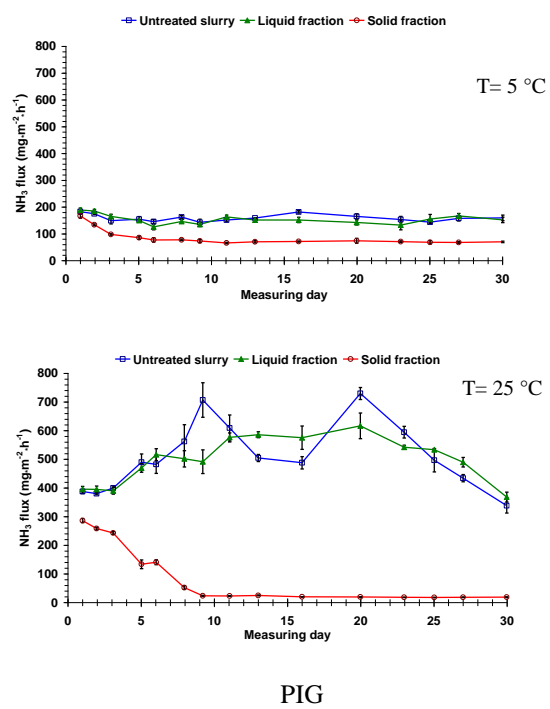
405 Fig. 2.

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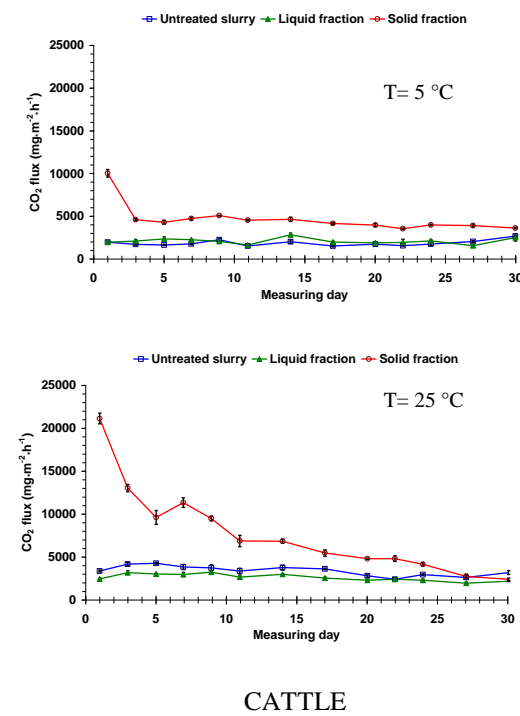
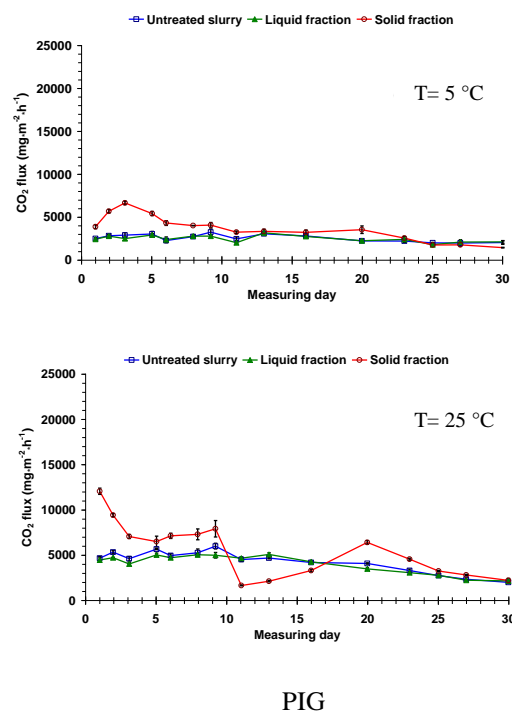


407 Fig. 3.

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410 Fig. 4.  
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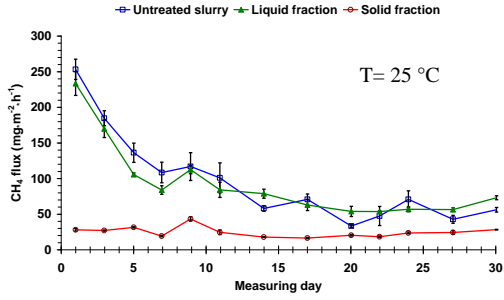
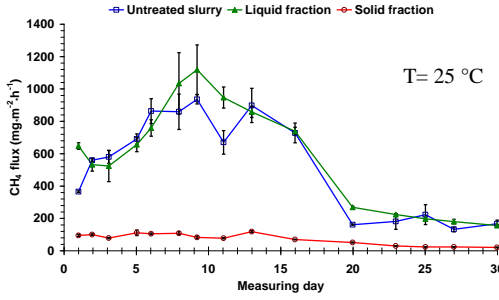
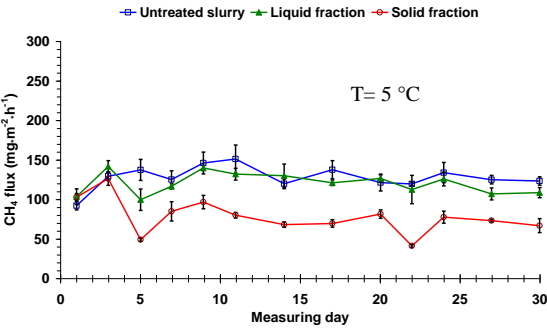
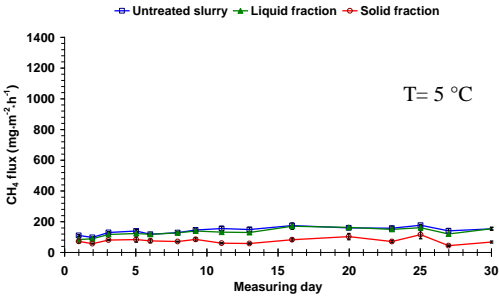
413 Fig. 5.

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PIG

CATTLE

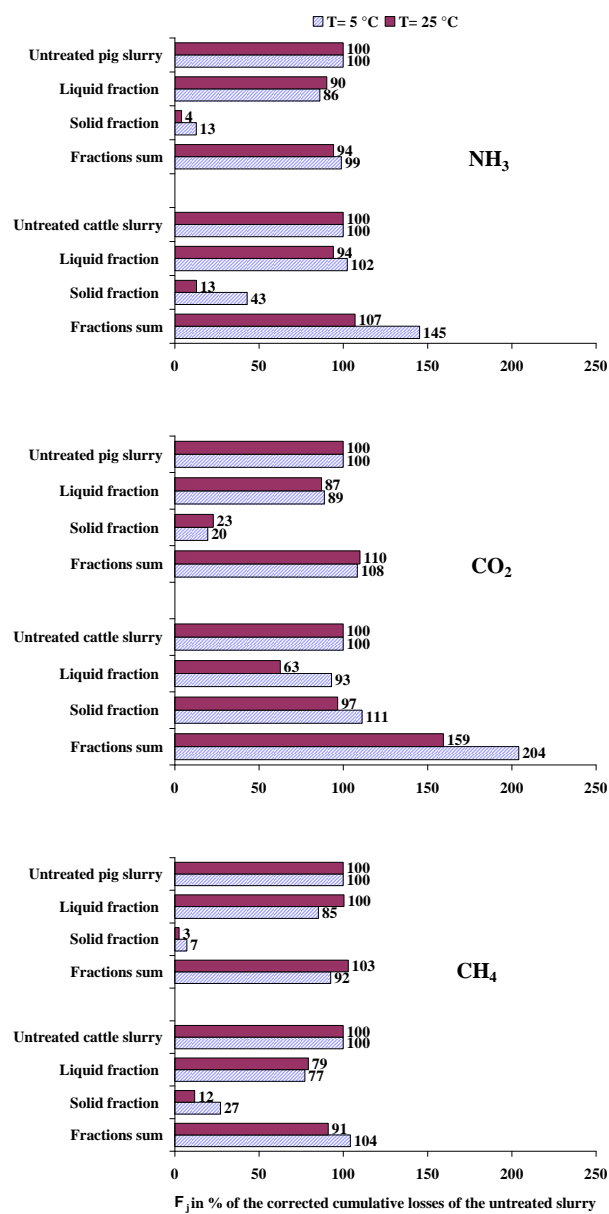
418 Fig. 6.

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423 Fig. 7.

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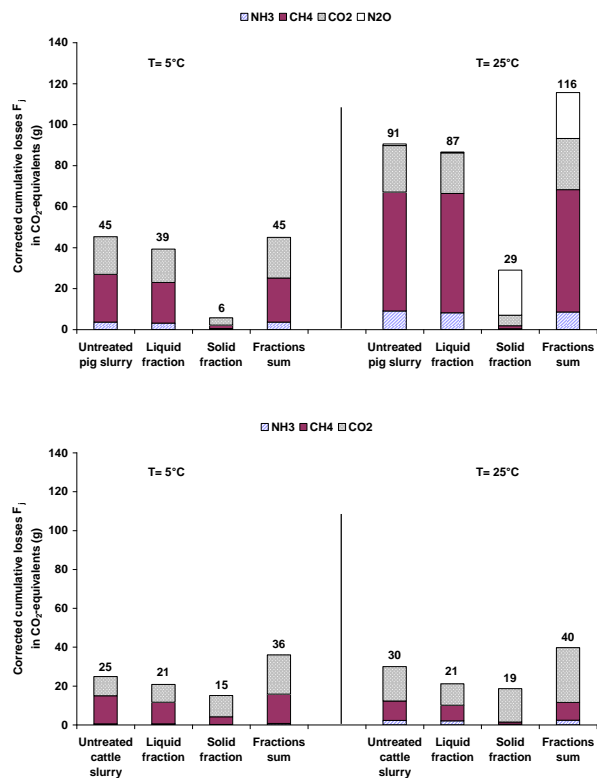
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434 Fig. 8.  
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436 **Table legends**

437 Table 1. Main composition of the manures at the beginning of each experiment

438 (n=2) and the correction factors  $\rho$  used for  $\Phi_j$  calculation.

439 Table 2. Main composition of the manures at the end of each experiment (n=4) and volume reductions over the storage  
440 period.

441 Table 3. Mean gaseous losses from each of the tested material occurred at the different experimental conditions after 30  
442 d of storage.

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448 Table 1.

Type of slurry	Product	pH	TS %	VS %	TAN g kg <sup>-1</sup>	TKN g kg <sup>-1</sup>	Org. Acids %	$\rho$
Pig	Untreated slurry	7.79	5.90	4.21	4.31	6.40	4.78	1.00
	Liquid fraction	7.86	4.65	3.01	4.33	5.90	3.15	0.92
	Solid fraction	8.82	21.1	19.1	4.05	12.2	3.47	0.20
Cattle	Untreated slurry	7.11	7.46	6.02	1.47	3.58	4.48	1.00
	Liquid fraction	7.09	5.12	3.81	1.49	3.59	5.80	0.82
	Solid fraction	8.35	19.2	17.3	1.16	2.65	4.18	0.45

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452 Table 2.

Type of slurry	Storage temperature °C	Product	pH	TS %	VS %	TAN g kg <sup>-1</sup>	N Kjel. g kg <sup>-1</sup>	Org. Acids %	Volume reduction %
Pig	25	Untreated slurry	8.43	8.38	5.31	1.55	4.10	1.46	46.3
	25	Liquid fraction	8.50	6.32	3.39	1.46	3.79	2.23	46.3
	25	Solid fraction	7.25	28.6	25.0	0.28	6.63	1.29	0.00
	5	Untreated slurry	7.92	5.98	4.16	3.65	5.76	3.26	3.72
	5	Liquid fraction	7.95	4.69	2.93	3.70	5.74	4.07	7.48
	5	Solid fraction	8.79	23.9	21.7	2.82	3.13	1.48	7.48
Cattle	25	Untreated slurry	6.96	8.63	6.76	1.51	3.22	8.48	38.4
	25	Liquid fraction	7.30	5.74	3.89	1.30	2.90	6.66	34.5
	25	Solid fraction	8.29	22.1	18.3	0.05	5.87	0.82	30.6
	5	Untreated slurry	6.79	7.67	6.17	1.40	3.32	6.37	3.72
	5	Liquid fraction	6.96	4.99	3.64	1.43	3.23	5.68	7.48
	5	Solid fraction	8.47	18.6	16.3	0.20	3.57	0.80	3.72

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Table 3.

Type of slurry	Temperature °C	Untreated slurry				Liquid fraction				Solid fraction			
		N-NH <sub>3</sub> (%TKN)	N-N <sub>2</sub> O (%TKN)	C-CH <sub>4</sub> (%VS)	C-CO <sub>2</sub> (%VS)	N-NH <sub>3</sub> (%TKN)	N-N <sub>2</sub> O (%TKN)	C-CH <sub>4</sub> (%VS)	C-CO <sub>2</sub> (%VS)	N-NH <sub>3</sub> (%TKN)	N-N <sub>2</sub> O (%TKN)	C-CH <sub>4</sub> (%VS)	C-CO <sub>2</sub> (%VS)
Pig	5	15.1 a	ND	3.34 a	20.0 a	15.0 a	ND	4.39 a	27.4 a	7.12 a	ND	0.68 a	11.1 a
		(0.34)		(0.05)	(0.41)	(0.61)		(0.17)	(0.68)	(0.04)		(0.02)	(0.37)
	25	37.8 b	ND	8.53 b	25.6 b	40.8 b	ND	12.8 b	33.4 b	5.57 b	4.71	0.60 b	16.3 b
		(0.57)		(0.43)	(0.64)	(0.22)		(0.47)	(0.35)	(0.11)	(0.12)	(0.02)	(0.26)
Cattle	5	3.60 c	ND	1.56 c	7.66 c	4.63 c	ND	2.19 c	13.7 c	5.21 c	ND	0.77 c	16.4 cb
		(0.09)		(0.05)	(0.19)	(0.14)		(0.10)	(0.42)	(0.10)		(0.01)	(0.36)
	25	16.5 d	ND	1.01 d	13.7 d	18.4 d	ND	1.55 d	16.7 d	6.03 db	ND	0.23 d	25.6 d
		(0.17)		(0.04)	(0.33)	(0.36)		(0.08)	(0.17)	(0.25)		(0.00)	(0.45)

Error standards are given in parentheses (n=4). Means with unequal letters in each column are significantly different (P<0.05).

ND = not detected